IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for removing [[N2O]] $\underline{N_2O}$ in nitric acid manufacture, which comprises utilizing catalysts comprising contacting a gas mixture comprising $\underline{N_2O}$ and at least one other gas with at least one catalyst comprising wire wovens and/or drawn-loop knits composed comprised of high-temperature-stable materials [[and]] coated with catalytically active materials.

Claim 2 (Currently Amended): [[A]] The process for removing N₂O in nitric acid manufacture according to claim 1, wherein the wire wovens and/or drawn-loop knits comprise Fe-Cr-Al alloys coated with catalytically active materials consist of Fe Cr-Al alloys.

Claim 3 (Currently Amended): The process for removing N_2O in nitric acid manufacture according to claim 1, wherein the wire or the wire wovens and/or drawn-loop knits composed of comprising high-temperature-stable materials are heat treated at from 100 to 1500°C prior to coating.

Claim 4 (Currently Amended): The process for removing N_2O in nitric acid manufacture according to claim 1, wherein the wire woven and/or drawn-loop knit coated with catalytically active materials forms a catalyst bed from 1 to 150 cm deep.

Claim 5 (Currently Amended): The process for removing N_2O in nitric acid manufacture according to claim 1, wherein the temperature at the wire woven and/or drawn-

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loop knit coated with catalytically active materials is located in a reactor where the temperature is in the range from 500 to 980°C.

Claim 6 (Currently Amended): The process for removing N₂O in nitric acid manufacture according to claim 1, wherein the residence time of the nitrogen oxides within over the wire woven and/or drawn-loop knit coated with catalytically active materials is less than 1 second.

Claim 7 (Currently Amended): A catalyst for removing N₂O in nitric acid manufacture, constructed of a wire woven and/or drawn-loop knit composed of comprising high-temperature-stable materials [[and]] coated with catalytically active materials.

Claim 8 (Currently Amended): A reactor for catalytic oxidation of ammonia to nitrogen oxides which comprises a noble metal catalyst, an optional noble metal recovery network, and a heat exchanger in the stated order in the flow direction, wherein a wire woven and/or drawn-loop knit eomposed of comprising high-temperature-stable materials [[and]] coated with catalytically active materials is disposed between the noble metal catalyst/optional noble metal recovery network and the heat exchanger.

Claim 9 (Previously Presented): An apparatus for producing nitric acid from ammonia, comprising in the stated order

- a) a reactor according to claim 8,
- b) an absorption unit for absorbing nitrogen oxides in an aqueous medium, and if appropriate
 - c) a reduction unit for selective catalytic reduction of nitrogen oxides.

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Claim 10 (New): The process for removing N_2O according to claim 1, wherein the gas mixture comprising N_2O and at least one other gas is a by-product of nitric acid production.

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